## HMA-2 <br> MA-2

Patent Pending
\#10/306,199

## The Blue Flame Series

DIRECT FIRED MAKE-UP AIR BURNERS are used in industrial and commercial applications to maintain the desired environmental temperatures required by critical processes i.e. health purposes, production systems, quality control, comfort and loss prevention where it is necessary or required to exhaust large amounts of conditioned air.

Make-up Air Systems used as stand alone heating systems or operating in combination with central heating plants systems can be cost effective in three ways: 1) reducing the initial expenditures, 2) tempering incoming air which may extend the life of expensive central heating plants and 3) reducing excessive equipment cycling or premature component failures due to increased heating demands.

## New Technology in Direct-Fired Gas Burners

Our innovative two stage combustion burner is not just a modification or improvement of the old, but a completely new approach to direct-fired combustion. The two-stage combustion improves control of the flame process, meets or exceeds the new ANSI Standards while outperforming the competition. By incorporating two separate flames within the burner combustion zone, the flame is more stable, shorter and cleaner, permitting the reduction of emissions levels and allowing for higher temperature rise and higher tolerance to varying conditions when placed in the profile opening.

- Reduced $\mathrm{NO}_{2}$ and CO Emissions: Lower emissions levels that easily pass the new ANSI Z83.4 and Z83.18 standards.
- Higher Temperature Rise: The two stage combustion process lowers $\mathrm{NO}_{2}$ emissions which is the limiting factor in temperature rise. (See page 3)
- Increased Capacity: Up to 750,000 BTU'S per foot. (Higher BTU levels can be achieved if ANSI Z83 Standards for CO and $\mathrm{NO}_{2}$ emissions are not of a concern. Process heaters can fire up to 1,000,000 BTU'S a foot or more.)
- Increased Differential Pressure Drop and Higher Velocities: HMA-2 burners can operate between 0.05 " to 1.4" W.C. differential pressure range or in air velocity between 800 fpm to 4000 fpm .
- Flame Stability: Two stage combustion provides better flame stability and emission control, allowing for a shorter flame and easier profile configuration.
- Reduced Inventory Costs: Single burner casting can be fired with natural, propane or butane gas ${ }^{1}$, reducing burner inventory.
- Reduced Shipping Costs: A smaller, lighter casting than the competition's, can cut your freight costs up to 50\%.
- Turndown: 30-1 turndown can easily be achieved with proper modulating controls and valves. (Higher turndown possible depending on equipment design.)
${ }^{1}$ Consult Midco for applications using butane fuels.


## Specifications

| *Firing Rate ..................................................... | Up to 750,000 Btu/hr/ft 750,000 + Contact Midco |
| :---: | :---: |
| Burner Manifold Pressure |  |
| Natural Gas | 4.2 to 8 inch W.C. |
| Propane Gas ................ | 1.6 to 3 inch W.C. |
| Pilot Capacity ............................................... | 12,000 Btu/hr |
| Pilot Manifold Gas Pressure |  |
| Natural Gas | 3.5 inch W.C. |
| Propane Gas | 2.0 inch W.C. ** |
| Pressure Drop Across the Burner | 0.05 to 1.4 inch W.C. |
| Air Velocity Across the Burner | 800 to 4,000 FPM |
| Burner Turn-down Ratio ....................................... | 30 to 1 |
| Flame Length ...................................................... | 10 inches at a full firing rate |

* Firing rate is dependent on the pressure across the burner. Please see the included charts for recommended burner sizing.
** Using a natural gas pilot on propane.

| *Burner Configurations | *Pilot Configurations |  |  |
| :---: | :---: | :---: | :---: |
|  | Part \# |  | Part \# |
| 6 inch Straight Section (15.24cm) | 1050700 | Spark rod and flame rod | 1190800 |
| 6 inch Straight Section with Back Inlet (15.24cm) | 1230700 | Spark rod and UV | 1200300 |
| 12 inch Straight Section (30.48cm) | 1010700 | Remote flame rod | 1220800 |
| 12 inch Straight Section with Back Inlet(30.48cm) | 1060700 | Remote UV | 1240800 |
| Elbow Section | 1070700 | Pilot with spark rod only | 1210800 |
| Tee Section | 1080700 | Flame rod | 1360-03 |
|  |  | Spark rod | 1342-00 |

Table 1 - Burner and Pilot Configurations

* See Page 15, Figure 1b for configuration reference.

Midco International Inc. reserves the right to change the construction or configuration of its products at any time.

All information is based on laboratory testing. Different unit size and/or configurations may affect data.


750,000 Btu/hr/ft at 1.4 " W.C. pressure drop across the burner


550,000 Btu/hr/ft at 0.6 " W.C. pressure drop across the burner


350,000 Btu/hr/ft at 0.2 " W.C. pressure drop across the burner

$750,000 \mathrm{Btu} / \mathrm{hr} / \mathrm{ft}$ at 1.4 " W.C. pressure drop across the burner


550,000 Btu/hr/ft at 0.6 " W.C. pressure drop across the burner

$350,000 \mathrm{Btu} / \mathrm{hr} / \mathrm{ft}$ at 0.2 " W.C. pressure drop across the burner

Chart 1 - CO and $\mathrm{NO}_{2}$ Emissions Data
*For temperature rise up to $160^{\circ} \mathrm{F}$ that meets the ANSI Z83 standards contact Midco.


Chart 2 - BTU's verses Pressure Drop


Chart 3-BTU's verses Gas Pressure (" W.C.)


Chart 4 - Pressure Across the Burner verses Profile Velocity

Profile Setup

Profile Setup Example

1. Required BTU:

BTU/hr $=$ Blower SCFM $\times$ Desired Temp. Rise $\times 1.08$
2. Required Burner Length:

Feet of burner $=[$ Required $B T U / h r] \div[$ Burner Firing Rate (BTU/hr/ft)]
The Burner Firing Rate should correspond to the pressure drop across the burner shown in Chart 2.
3. Required Profile Area:

Total Burner Area $=$ Number of burner sections $\times$ burner area

| (Burner Section) | Burner Area |
| :--- | :--- |
| 6 inch | 0.32 sq. ft. |
| 12 inch | $0.65 \mathrm{sq} \mathrm{ft}$. |
| T Section | $0.77 \mathrm{sq} \mathrm{ft}$. |
| Ell Section) | $0.65 \mathrm{sq} \mathrm{ft}$. |

Net Profile Area = Rated Fan (SCFM) $\div$ Profile Velocity (SFPM)
The Profile Velocity can be determined from the following:

$$
\text { Profile Velocity }=945 \sqrt{\frac{\Delta P}{0.075}}
$$

$\Delta \mathrm{P}$ is the pressure drop across the burner
Profile Area $=$ Net Profile Area + Total Burner Area

Sizing the burner and the corresponding profile for a 5,000 SCFM and a 115 degrees temperature rise.

1. Required BTU:

BTU/hr $=$ Blower SCFM $\times$ Desired Temp. Rise $\times 1.08$
$B T U / h r=5,000(S C F M) \times 115(\Delta T) \times 1.08=621,000 B T U / h r$
2. Required Burner Length:

Feet of burner $=[$ Required $\mathrm{BTU} / \mathrm{hr}] \div[$ Burner Firing Rate $(\mathrm{BTU} / \mathrm{hr} / \mathrm{ft})]$
To determine the optimum burner length we can choose from a combination of 12 inch or 6 inch burner sections referring to Table 1. We can either fire the burner at a rate of $621,000 \mathrm{BTU} / \mathrm{hr}$ per ft , or we can fire the burner at $414,000 \mathrm{BTU} / \mathrm{hr}$ per ft ( 1.5 feet of burner). Refer to Chart 3 for the fuel pressures requirements at different firing rates.
3. Required Profile Area:

Total Burner Area $=$ Number of burner sections $\times$ burner area

| (Burner Section) | Burner Area |
| :--- | :--- |
| 6 inch | 0.32 sq. ft. |
| 12 inch | 0.65 sq. ft. |
| T Section | 0.77 sq. ft. |
| Ell Section | 0.65 sq. ft. |

[^0]
## Installation

Profile Setup Example Continued

Net Profile Area $=$ Rated Fan $(S C F M) \div$ Profile Velocity $($ SFPM $)$
The Profile Velocity should be determined based on the burner firing rates. If we choose to fire the burner at 621,000 BTU/hr/ft then the profile opening should be sized for a pressure drop of 0.8 inch W.C. across the burner. If the firing rate is $414,000 \mathrm{BTU} / \mathrm{hr} / \mathrm{ft}$ then the profile opening should be sized for a pressure drop of 0.4 inch W.C. across the burner. The corresponding profile velocity across the burner should be determined from Chart 4 or use the following equation.

$$
\text { Profile Velocity }=945 \sqrt{\frac{\Delta P}{0.075}}
$$

For the 621,000 BTU/hr/ft

$$
\text { Profile Velocity }=945 \sqrt{\frac{0.8}{0.075}}=3086(S F P M)
$$

Net Profile Area $=5000($ SCFM $) \div 3086($ SFPM $)=1.62 \mathrm{ft}^{2}$
For the 414,000 BTU/hr/ft

$$
\text { Profile Velocity }=945 \sqrt{\frac{0.4}{0.075}}=2182(\text { SFPM })
$$

Net Profile Area $=5000($ SCFM $) \div 2182($ SFPM $)=2.29 \mathrm{ft}^{2}$
To calculate the profile area needed for both cases:
Profile Area $=$ Net Profile Area + Total Burner Area
For the $621,000 \mathrm{BTU} / \mathrm{hr} / \mathrm{ft}$
Profile Area $=1.62+0.650=2.27 \mathrm{ft}^{2}$
For the 414,000 BTU/hr/ft
Profile Area $=2.29+0.975=3.265 \mathrm{ft}^{2}$
To calculate the length of the profile opening add burner length to the desired clearance:
For the 621,000 BTU/hr/ft case
12 inch +4 inch ( 2 inch on each side) $=16$ inch (1.3ft)
For the 414,000 BTU/hr/ft case
18 inch +4 inch ( 2 inch on each side ) $=22$ inch (1.83ft)
To calculate the height of the profile opening divide the profile area by the profile length:
For the $621,000 \mathrm{BTU} / \mathrm{hr} / \mathrm{ft}$ case
$2.27 \mathrm{ft}^{2} \div 1.3 \mathrm{ft}=1.75 \mathrm{ft}(21 \mathrm{inch})$
For the 414,000 BTU/hr/ft case
$3.265 \mathrm{ft}^{2} \div 1.83 \mathrm{ft}=1.78 \mathrm{ft}(21.5 \mathrm{inch})$

IMPORTANT: Furnace cement must be used to join and seal all burner casting sections, and end flanges only. If this procedure is not performed, gas leakage will occur. Use $10-24 \times 3 / 8$ stainless steel screws and nuts or stainless steel rivets. UNDER NO CIRCUMSTANCES SHOULD STANDARD GRADE HARDWARE OR ALUMINUM RIVETS BE USED.

When assembling Make-Up Air Burners, a few simple but important assembly procedures must be followed to insure Burner Performance. Care should be taken when removing, assembling and placing the burner into the heater.

1. Examine the baffles for structural integrity; only new undamaged components should be used.
2. Assemble individual burner cast iron sections first.
3. When joining the baffle sections to the burner casting, place a gasket between the casting and the baffles, do not tighten the cast iron sections until the entire unit is assembled. Baffles can be riveted together with stainless steel rivets or joined with stainless steel screws.
4. Prepare a mixture of furnace cement thinned to the consistency of a heavy cream.
5. Apply furnace cement to both mating surfaces of the burner castings and end flanges only.
6. After sections are joined, wipe off excess furnace cement and make sure you do not clog any gas or air ports.
7. After all baffle plates are tight, secure all baffle plates to the burner casting. Make sure all bolts and rivets are tight.
8. After all sections are assembled, check for potential gas or air leaks. If necessary, close up any remaining gaps with furnace cement.
9. For high fire start systems, the first adjacent gas port hole (next to the pilot) should be plugged with furnace cement. See Figure 8 -Pilot Configuration.

## Burner Placement in the Profile

The performance of the HMA-2 burner depends on the unit in which the burner is located. The burner can perform differently in different units and can obtain different end results. Maintaining a relative laminar flow around the burner and providing a sufficient space between the burner and the blower is a key factor in obtaining best burner performance. The unit should be free of any obstructions that can create turbulent effect on the air.

The burner performance is highly dependent on its application and installation in the heater. Factors such as airflow around the burner, burner positioning in the profile, as well as, the profile sizing have high influence on the final emissions levels. Midco does not guarantee combustion results prior to performing actual combustion tests.

The burner should be located in the center of the profile. The profile clearance from ends of the burner should be kept at approximately 1 to 4 -inches. Typically setting the profile 2 " from the end plates is recommended. Any reinforcements used on the edge of the profile opening should be on the downstream side of the profile. The burner can be mounted either vertically or horizontally. Since the airflow varies from unit to unit best results should be determined by actual testing.


Note: Any reinforcements around the profile plates should be down stream of the profile plate

Figure 1a - Burner Placement in the Profile

Pull-Thru System


Figure 1b - Burner Placement in the Profile


Figure 2a - Pull-Thru System
The HMA-2 Burner is designed to operate in a make-up air heater and in an air stream taken directly from outdoors. To avoid stratification of the heated air, the burners should be located on the intake side center to the blower. Such positioning will take advantage of the blower mixing effect and ensure minimum temperature stratification. It will also allow for a relatively uniform airflow across the burner resulting in a clean combustion.

The total pressure of the blower must include allowance for the resistance of the heater and pressure drop across the burner, together with pressure losses at the inlet screen, inlet louvers, filters, plus the external pressure rating of the heater, if any. Contact equipment manufacturer for proper information.


Push-Thru System
The HMA-2 Burner will operate satisfactorily when located downstream of the blower. A mixing plenum may be required at the heater discharge opening to insure minimum temperature stratification. Blower and motor selection must be made on the basis of corrections for the coldest anticipated inlet temperature. In the push-thru system the heater outlet CFM will vary due to the expansion of air.


Figure 3-Push-Thru System


Elbow Duct Limits
Figure 4 - Installation in a Duct


Figure 5a - Gas Train Assemblies


Figure 5b-Direct Spark Gas Train Assemblies

Gas Inlet Capacities
Maximum Feet of Burner
Inlet Size Natural Propane Mfd.

| 1.5 " NPT End Inlet | $4^{\prime}$ | $5^{\prime}$ | $3^{\prime}$ |
| :--- | :---: | :---: | :---: |
| 2" NPT Back Inlet <br> Centrally Located | $6.5^{\prime}$ | $8^{\prime}$ | $4.5^{\prime}$ |

Table 2 - Gas Inlet Capacities

Burner Installation

Burner operation depends on the unit control setup in which the HMA-2 burner is used. A typical setup should consist of a Flame Safety Control with appropriate air flow proving system and a Modulating Gas Control System.

1. Verify the pressure across the burner. The pressure across the burner can be measured by placing two static pressure probes, one downstream and one upstream of the profile opening and measure the differential pressure. The pressure should be within burner operating specifications and within the expected calculated pressure.
2. With the burner off check the Flame Safety Air Proving System
a. Check the operation of the air proving system for low and high airflow setting. Refer to the Specifications of the Flame Safety Control for setup instructions and air switch operational characteristics.
3. Adjust the main gas pressure regulator to the pressure needed for the high fire according to Chart 3. Take into account pressure drops thru the gas valves and other components in the valve train.
4. For continuous, intermittent, or interrupted ignition systems
a. Pipe the pilot gas supply line up stream of the main gas valve.
b. Adjust the pilot pressure regulator to 3.5 inch W.C. for Natural Gas or 2.0 inch W.C. for propane gas.
5. For direct spark ignition system
a. Pipe the pilot gas supplied line to the main gas line downstream of the main gas valve.
b. Adjust the pilot pressure regulator to 3.5 inch W.C. for Natural Gas or 2.0 inch W.C. for propane gas.
6. Depending on the pilot configuration make following adjustments.
a. For Spark rod and flame rod configurations Make sure the flame rod is pointing towards burner manifold. Make sure the flame rod is not touching baffles or burner manifold. Make sure the spark rod is positioned above the pilot gas tube and that it will spark to the end of the gas tube. See Pilot Detail Drawings for this setting on page 16.
b. Spark rod and UV

Make sure the spark rod is positioned above the pilot gas tube and that it will spark to the end of the gas tube.
7. Pilot ignition
a. Make sure the main gas valve to the burner is closed for intermittent or interrupted ignition.
b. Observe the pilot flame, the flame should be blue and should extend approximately to the half of the burner end plate.
c. Check the flame signal.
8. Main burner ignition

Close the manual gas valve.
a. Set the Modulating Gas Control System to high fire position.

- Slowly open the manual gas valve.
- Observe the flame at high fire; the flame should be blue approximately 10 to 12 inches long. If the flame is long, lazy and orange the air to fuel ratio is not correctly adjusted. The pressure across the burner should be increased, refer to Chart 2.
- Check the flame signal.
- Check the manifold pressure to the corresponding firing rate. If the manifold pressure does not correspond to the pressures shown in Chart 3. Check for gas leaks.
Close the manual gas valve.
b. Set the Modulating Gas Control System to low fire position. Slowly open the manual gas valve.
- The flame should be evenly extending in the burner.
. The flame should be located in the casting of the burner.
- Check the flame signal.

Burner Installation Continued

For a high fire start system the first gas port next to the pilot might require to be blocked using furnace cement to prevent potential pilot blow outs and flame failures. See page 7 (Burner Assembly) and see Figure 8 - Pilot Configuration.

Slight redness and warpage of the baffle plates may occur at the high and intermediate fire inputs. This will not harm the burner. Once an initial discoloration and warp has taken ("set") no further permanent change will take place.

If the end plates redness occurs during high and intermediate fire inputs, the distance between the end plates and the profile opening might not be sufficient for the air to cool the end plates. Profile readjustments might be necessary.

## Burner Maintenance

## Trouble Shooting

I.
III.

The Midco HMA-2 Burner is only a component of the complete system. For trouble shooting of the equipment contact the OEM (Original Equipment Manufacturer) or the component manufacturer.
II. If the pilot fails to light, install a manometer on the pilot pressure tap. Check for 3.5" W.C. for natural gas or $2^{\prime \prime}$ W.C. for propane. If no gas check for voltage to pilot solenoid valve. If no voltage check operating controls or primary flame safeguard. If voltage to pilot solenoid valve is present and if there is 3.5 " W.C. gas pressure at pilot pressure tap then check for spark or flame rod settings. If there is no voltage to pilot solenoid valve, refer to Flame Safety control specifications or contact the original equipment manufacturer.

If Main Burner fails: If no main flame check manifold pressure. If no manifold pressure check for voltage to the gas solenoid valve and check if main manual valve is open. If no voltage to gas valve refer to Flame Safety control specifications or contact the original equipment manufacturer.
IV. If the pilot fails as main gas valves open, the first adjacent gas port hole (next to the pilot) should be plugged with furnace cement. See Figure 8 - Pilot Configuration.

1. Make sure the system is off
2. Inspect the burner baffles for plugged openings
a. Clean baffles with wire brush
b. Make sure the baffles are tightly attached to each other and to the burner casting.
3. Inspect the burner casting for plugged openings
a. Clean casting with wire brush
b. If necessary re-drill gas ports with a $1 / 8^{\prime \prime}\left(0.125^{\prime \prime}\right)$ drill size and air ports with a number 43 (0.089") drill size.
4. Turn the system on and visually inspect the flame.
5. For Service Bulletins on the cleaning and maintenance of burners contact Midco.


Figure 6 - Burner Sections - Assembly

Table 3 - Burner Assembly Parts List

## Parts - Pilot Configuration \& Mounting / Equation Reference



Figure 8 - Pilot Configuration

## Equation Reference

1. Conversion of SCFM to Actual CFM of air

SCFM $=$ CFM $\times \frac{\rho}{0.075}$
2. Air density as a function of Temperature -- $\rho=1.35 \times \frac{\text { Barometric Pressure (in } \mathrm{Hg} \text { ) }}{T_{\text {(out) }}+460}$
3. Change in Standard Barometric Pressure as a function of Altitude

Barometric Pressure $(\mathrm{in} . \mathrm{Hg})=29.921 \times(1-6.8753 \times 0.000001 x \text { altitude }(\mathrm{ft}))^{\wedge} 5.2559$
4. Temperature difference -- Temperature Rise $=T_{\text {(out) }}-T_{\text {(in) }}$
5. Energy equation - BTU/hr $=$ SCFM $\times$ Temperature Rise $\times 1.08$

Where: 1.08 is a sensible heat equation constant

$$
1.08=0.2397\left(\frac{B T U}{l b}\right) \times 60\left(\frac{m i n}{H}\right) \times 0.075\left(\frac{l b}{f^{3}}\right)
$$


[^0]:    Total Burner Area $=1.0(\mathrm{ft}) \times 0.65=0.650 \mathrm{ft}^{2}$ Or

    Total Burner Area $=1.5(\mathrm{ft}) \times 0.65=0.975 \mathrm{ft}^{2}$

